

Research Article

Soret and Dufour Effects on Natural Convection Flow Past a Vertical Surface in a Porous Medium with Variable Viscosity

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The heat and mass transfer characteristics of natural convection about a vertical surface embedded in a saturated porous medium subject to variable viscosity are numerically analyzed, by taking into account the diffusion-thermo (Dufour) and thermal-diffusion (Soret) effects. The governing equations of continuity, momentum, energy, and concentrations are transformed into nonlinear ordinary differential equations, using similarity transformations, and then solved by using Runge-Kutta-Gill method along with shooting technique. The parameters of the problem are variable viscosity, buoyancy ratio, Lewis number, Prandtl number, Dufour effect, Soret effect, and Schmidt number. The velocity, temperature, and concentration distributions are presented graphically. The Nusselt number and Sherwood number are also derived and discussed numerically.

1. Introduction

Coupled heat and mass transfer by natural convection in a fluid-saturated porous medium has received great attention during the last decades due to the importance of this process which occurs in many engineering, geophysical, and natural systems of practical interest such as geothermal energy utilization, thermal energy storage, and recoverable systems and petroleum reservoirs. A comprehensive account of the available information in this field is provided in recent books by Pop and Ingham [1], Ingham and Pop [2], and Vafai [3].

The previous studies, dealing with the transport phenomena of momentum and heat transfer, have dealt with one-component phases which possess a natural tendency to reach equilibrium conditions. However, there are activities, especially in industrial and chemical engineering processes, where a system contains two or more components whose concentrations vary from point to point. In such a system, there is a natural tendency for

mass to be transferred, minimizing the concentration differences within the system and the transport of one constituent, from a region of higher concentration to that of a lower concentration. This is called mass transfer.

When heat and mass transfer occurs simultaneously between the fluxes, the driving potential is of more intricate nature, as energy flux can be generated not only by temperature gradients but by composition gradients as well. The energy flux caused by a composition gradient is called the Dufour or diffusion-thermo effect. Temperature gradients can also create mass fluxes, and this is the Soret or thermal-diffusion effect. Generally, the thermal-diffusion and the diffusion-thermo effects are of smaller-order magnitude than the effects prescribed by Fourier's or Fick's laws and are often neglected in heat and mass transfer processes. There are, however, exceptions. The Soret effect, for instance, has been utilized for isotope separation, and in mixtures between gases with very light molecular weight (H_2 , He). For medium molecular weight (N_2 , air), the Dufour effect was found to be of a considerable magnitude such that it cannot be neglected (Eckert and Drake) [4].

Kassoy and Zebib [5] studied the effect of variable viscosity on the onset of convection in porous medium. Cheng and Minkowycz [6] studied the effect of free convection about a vertical plate embedded in a porous medium with application to heat transfer from a dike. Bejan and Khair [7] studied the buoyancy-induced heat and mass transfer from a vertical plate embedded in a saturated porous medium. Lai and Kulacki [8] studied the coupled heat and mass transfer by natural convection from vertical surface in a porous medium. The same authors [9] also studied the effect of variable viscosity on convection heat transfer along a vertical surface in a saturated porous medium. Elbashbeshy and Ibrahim [10] investigated the effect of steady free convection flow with variable viscosity and thermal diffusivity along a vertical plate. Kafoussias and Williams [11] studied the thermal-diffusion and diffusion-thermo effects on the mixed free-forced convective and mass transfer steady laminar boundary layer flow, over a vertical plate, with temperature-dependent viscosity. Yih [12] analyzed the coupled heat and mass transfer in mixed convection about a wedge for variable wall temperature and concentration. Jumah and Mujumdar [13] studied the coupled heat and mass transfer for non-Newtonian fluids. Anghel et al. [14] investigated the Dufour and Soret effects on free convection boundary layer over a vertical surface embedded in a porous medium. Kumari [15] analyzed the effect of variable viscosity on free and mixed convection boundary layer flow from a horizontal surface in a saturated porous medium. Postelnicu et al. [16] investigated the effect of variable viscosity on forced convection over a horizontal flat plate in a porous medium with internal heat generation. Seddeek [17], Seddeek and Salem [18] studied the effects of chemical reaction, variable viscosity, and thermal diffusivity on mixed convection heat and mass transfer through porous media. Ali [19] studied the effect of variable viscosity on mixed convection along a vertical plate. Alam et al. [20] analyzed the study of the combined free-forced convection and mass transfer flow past a vertical porous plate in a porous medium with heat generation and thermal diffusion. Pantokratoras [21] analyzed the effect of variable viscosity with constant wall temperature. Partha et al. [22] looked for the effect of double dispersion, thermal-diffusion, and diffusion-thermo effects in free convection heat and mass transfer in a non-Darcy electrically conducting fluid saturating a porous medium. Alam and Rahman [23] studied the Dufour and Soret effects on mixed convective flow past a vertical porous plate with variable suction. Seddeek et al. [24] studied the effects of chemical reaction and variable viscosity on hydromagnetic mixed convection heat and mass transfer through porous media. Another contribution to the theme of Dufour and Soret effects can be found in the paper by Afify [25], where there is a non-Darcy free convection past a vertical surface with temperature viscosity.

Narayana and Murthy [26] studied the Soret and Dufour effects in a doubly stratified Darcy porous medium. Postelnicu [27] studied the influence of chemical reactions along with Soret and Dufour's effect in the absence of magnetic field on free convection. Singh and Chandarki [28] used integral treatment to obtain the expressions for Nusselt number and Sherwood number. El-Arabawy [29] studied the Soret and Dufour effects in a vertical plate with variable surface temperature. Postelnicu [30] analyzed the effect of Soret and Dufour on heat and mass transfer at a stagnation point. Tak et al. [31] investigated the MHD free convection-radiation in the presence of Soret and Dufour. Vempati and Laxmi-Narayana-Gari [32] studied the Soret and Dufour on MHD with thermal radiation. Recently, Cheng [33] studied the Soret and Dufour on heat and mass transfer on a vertical truncated cone with variable wall temperature and concentration. The aim of this paper is to study the effect of Soret and Dufour on heat and mass transfer by natural convection from a vertical plate with variable viscosity.

2. Analysis

Consider a vertical surface embedded in a saturated porous medium. The properties of the fluid and porous medium are isotropic, and the viscosity of the fluid is assumed to be an inverse linear function of temperature. Using Boussinesq and boundary layer approximations, the governing equations of continuity, momentum, energy, and concentration are given by

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (2.1)$$

$$u = -\frac{\kappa}{\mu} \left(\frac{\partial p}{\partial x} + \rho g \right), \quad (2.2)$$

$$v = -\frac{\kappa}{\mu} \left(\frac{\partial p}{\partial y} \right), \quad (2.3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} + \frac{D_m k_T}{c_s c_p} \frac{\partial^2 c}{\partial y^2}, \quad (2.4)$$

$$u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y} = D_m \frac{\partial^2 c}{\partial y^2} + \frac{D_m k_T}{T_m} \frac{\partial^2 T}{\partial y^2}, \quad (2.5)$$

$$\rho = \rho_\infty \{1 - \beta(T - T_\infty) - \beta^*(c - c_\infty)\}. \quad (2.6)$$

The viscosity of the fluid is assumed to be an inverse linear function of temperature, and it can be expressed as

$$\frac{1}{\mu} = \frac{1}{\mu_\infty} \{1 + \gamma(T - T_\infty)\}, \quad (2.7)$$

which is reasonable for liquids such as water and oil. Here, γ is a constant. The boundary conditions are

$$\begin{aligned} y = 0, & \quad v = 0, & \quad T = T_w, & \quad c = c_w, \\ y \rightarrow \infty, & \quad u = 0, & \quad T = T_\infty, & \quad c = c_\infty. \end{aligned} \quad (2.8)$$

3. Method of Solution

Introducing the stream function $\Psi(x, y)$ such that

$$u = \frac{\partial \Psi}{\partial y}, \quad v = -\frac{\partial \Psi}{\partial x}, \quad (3.1)$$

where

$$\Psi = \alpha f (\text{Ra}_x)^{1/2}, \quad (3.2)$$

$$\eta = \frac{y}{x} (\text{Ra}_x)^{1/2}, \quad (3.3)$$

$$\text{Ra}_x = \left\{ \frac{kg\beta\Delta T x}{\nu\alpha} \right\}, \quad \text{is the Rayleigh number} \quad (3.4)$$

Define

$$\theta = \frac{T - T_\infty}{T_w - T_\infty}, \quad (3.5)$$

$$\phi = \frac{c - c_\infty}{c_w - c_\infty}, \quad (3.6)$$

$$N = \frac{\beta^*(c_w - c_\infty)}{\beta(T_w - T_\infty)}. \quad (3.7)$$

Substituting these transformations (3.1) to (3.7) to Equations (2.2) to (2.5) along with (2.6) and (2.7), the resulting nonlinear ordinary differential equations are

$$f'' = \frac{f'\theta'}{\theta - \theta_r} - \left(\frac{\theta - \theta_r}{\theta_r} \right) (\theta' + \phi'N), \quad (3.8)$$

$$\theta'' + \text{Pr Du}\phi'' + \frac{1}{2}f\theta' = 0, \quad (3.9)$$

$$\phi'' + \text{Sc Sr}\theta'' + \frac{\text{Le}}{2}f\phi' = 0, \quad (3.10)$$

together with the boundary conditions

$$\begin{aligned} \eta = 0, & & f = 0, & & \theta = 1, & & \phi = 1, \\ \eta \rightarrow \infty, & & f' = 0, & & \theta = 0, & & \phi = 0, \end{aligned} \quad (3.11)$$

where $\text{Pr} = \nu/\alpha$ is the Prandtl number, $\text{Du} = D_m k_T (c_w - c_\infty) / c_s c_p \nu (T_w - T_\infty)$ is the Dufour number, $\text{Sc} = \nu/D_m$ is the Schmidt number, $\text{Sr} = D_m k_T (T_w - T_\infty) / T_m \nu (c_w - c_\infty)$ is the Soret number, $\text{Le} = \alpha/D_m$ is the Lewis number, and $\theta_r = -1/\gamma(T_w - T_\infty)$ is the parameter characterizing the influence of viscosity. For a given temperature differential, large values of

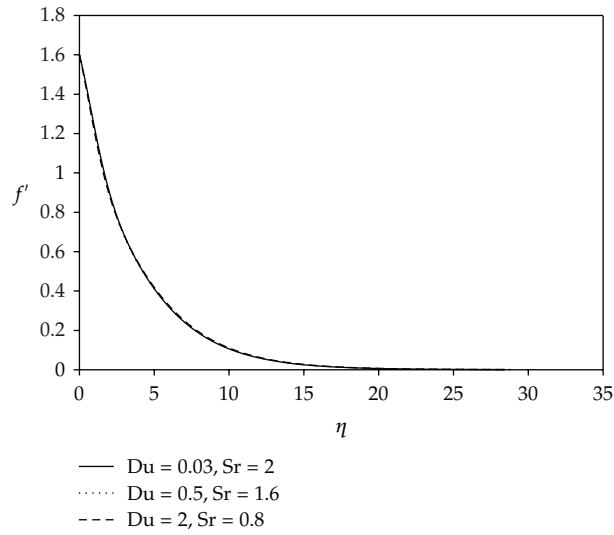


Figure 1: Velocity profile for different values of Dufour and Soret for $\theta_r = 5$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

θ_r imply that either γ or $(T_w - T_\infty)$ is small. In this case, the effect of variable viscosity can be neglected.

The effect of variable viscosity is important if θ_r is small. Since the viscosity of liquids decreases with increasing temperature while it increases for gases, θ_r is negative for liquids and positive for gases. The concept of this parameter θ_r was first introduced by Ling and Dybbs [34] in their study of forced convection flow in porous media. The parameter N measures the relative importance of mass and thermal diffusion in the buoyancy-driven flow. It is clear that N is zero for thermal-driven flow, infinite for mass-driven flow, positive for aiding flow, and negative for opposing flow.

4. Numerical Analysis and Discussion

Equations (3.8), (3.9), and (3.10) are integrated numerically by using Runge-Kutta-Gill method along with shooting technique. The parameters involved in this problem are θ_r : the variable viscosity, Le : Lewis number, N : the buoyancy parameter, Pr : Prandtl number, Du : Dufour number, Sr : Soret number, and Sc : Schmidt number. To observe the effect of variable viscosity on heat and mass transfer, we have plotted the velocity function f' , temperature function θ , and the concentration function Φ against η for various values of θ_r , Le , and N . The value of Prandtl number Pr is taken equal to 0.71 which corresponds to air. The values of the Dufour number and Soret number are taken in such a way that their product is constant according to their definition provided that the mean temperature is kept constant as well. The parameter θ_r is used to represent the effect of variable viscosity. The case $\theta_r < 0$ corresponds to the case of liquids, and $\theta_r > 0$ corresponds to the case of gases.

The influence of Dufour number Du and Soret number Sr on velocity, temperature, and concentration profiles is shown in Figures 1, 2, and 3, respectively, for $\theta_r = 5$, $N = 1$, $Le = 0.1$, $Pr = .71$, and $Sc = 0.1$. Figure 1 shows that as Dufour number increases, the velocity decreases slightly for decrease in Soret number. From Figure 2, it is evident that as Dufour

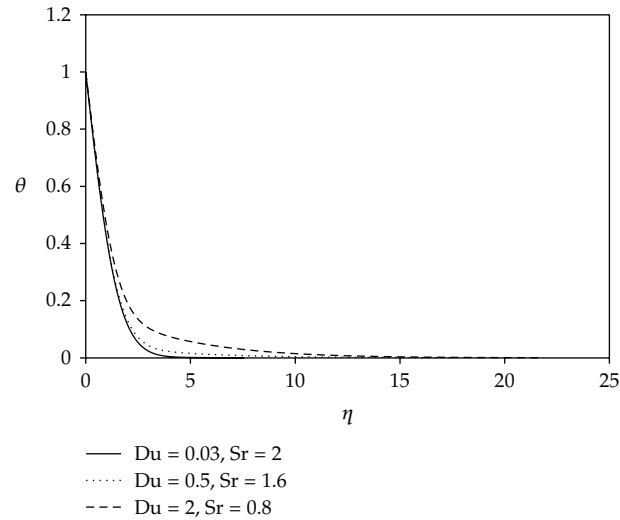


Figure 2: Temperature profile for different values of Dufour and Soret for $\theta_r = 5$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

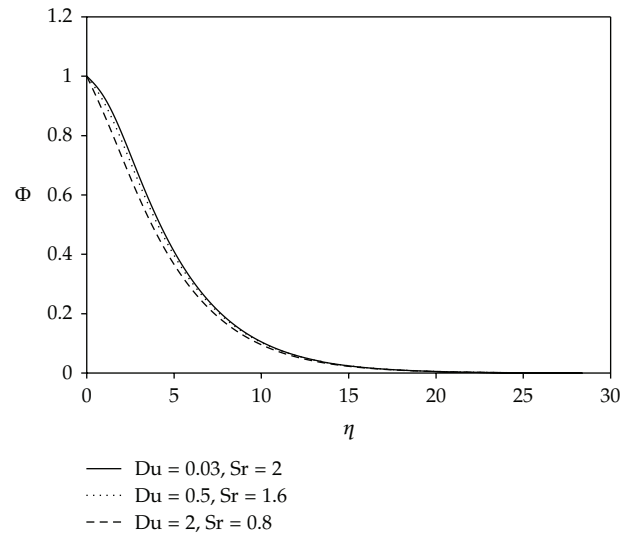


Figure 3: Concentration profile for different values of Dufour and Soret for $\theta_r = 5$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

number increases, the temperature increases for decrease in Soret number. Figure 3 shows that as Dufour number increases, the concentration decreases for decrease in Soret number.

The effect of variable viscosity θ_r on velocity, temperature, and concentration is shown in Figures 4, 5, and 6, respectively, for $N = 1$, $Le = 0.1$, $Pr = .71$, $Sc = 0.1$, $Du = 0.03$, and $Sr = 2$. From Figure 4, it is realized that the velocity increases near the plate and decreases away from the plate as $\theta_r \rightarrow 0$ in the case of liquids ($\theta_r < 0$) and decreases near the plate and increases away from the plate as $\theta_r \rightarrow 0$ in the case of gases ($\theta_r > 0$). From Figures 5 and 6, it is

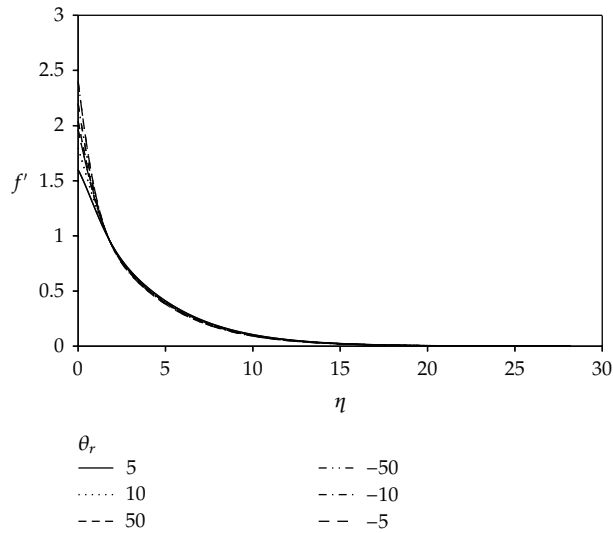


Figure 4: Velocity profile for different values of θ_r , for $Du = 0.03$, $Sr = 2$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

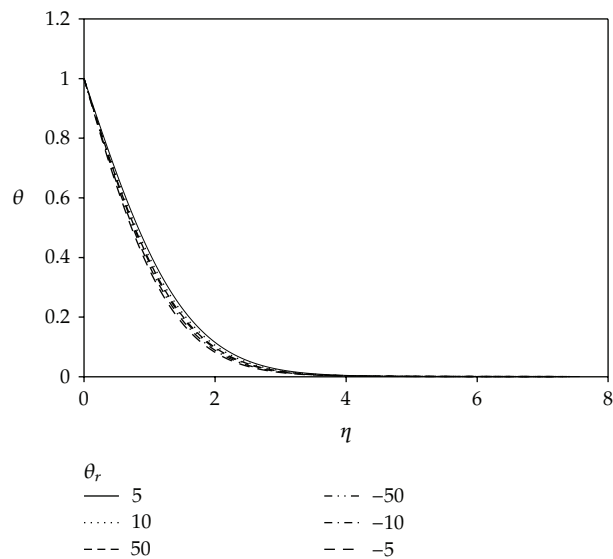


Figure 5: Temperature profile for different values of θ_r , for $Du = 0.03$, $Sr = 2$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

evident that the temperature and concentration increase as $\theta_r \rightarrow 0$ for $\theta_r > 0$ (i.e., for gases) and decrease as $\theta_r \rightarrow 0$ for $\theta_r < 0$ (i.e., for liquids).

The effect of buoyancy ratio N on velocity, temperature, and concentration is shown in Figures 7, 8, and 9, respectively, for $\theta_r = 5$, $Le = 0.1$, and $Pr = .71$ and $Sc = 0.1$, $Du = 0.03$, and $Sr = 2$. From Figure 7, it is observed that the velocity increases near the plate and decreases

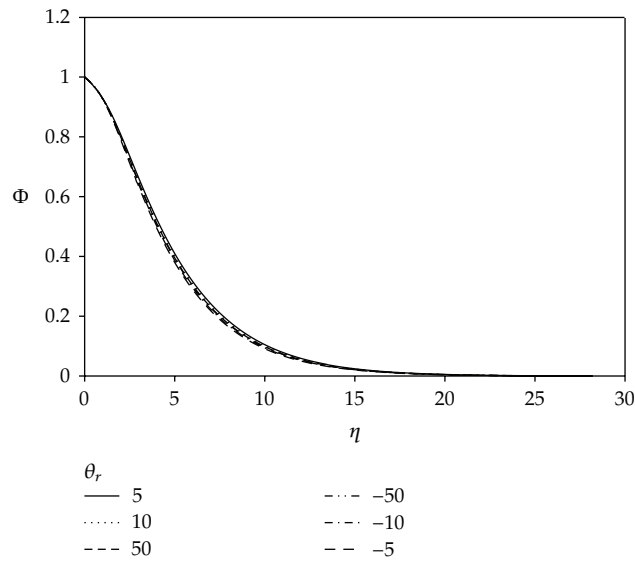


Figure 6: Concentration profile for different values of θ_r , for $Du = 0.03$, $Sr = 2$, $N = 1$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

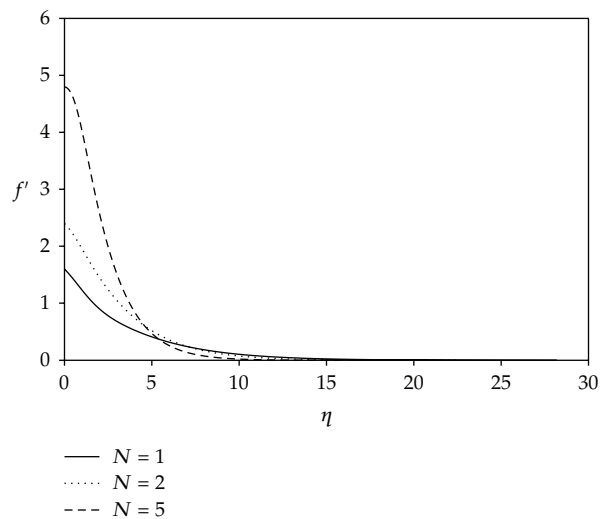


Figure 7: Velocity profile for different values of N for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

away from the plate as N increases. From Figures 8 and 9, it is realized that the temperature and concentration decrease as N increases.

The effect of Lewis number Le on temperature and concentration is shown in Figures 10 and 11, respectively, for $N = 1$, $Pr = .71$, $Sc = 0.1$, $Du = 0.03$, $Sr = 2$, and for different values of θ_r and Le . From Figure 10, it is observed that as Le increases, the heat

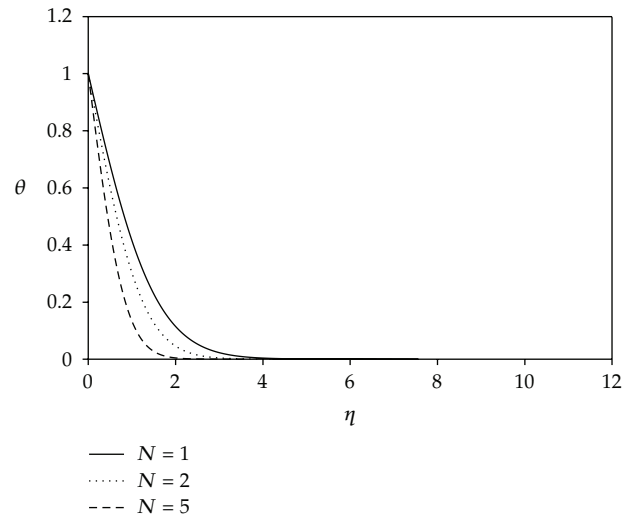


Figure 8: Temperature profile for different values of N for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

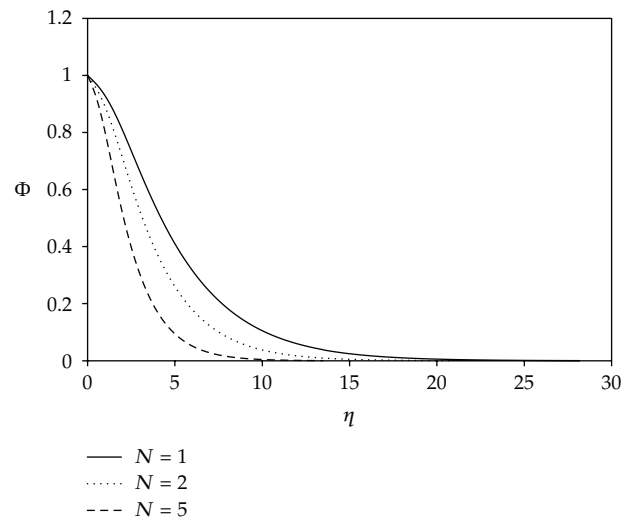


Figure 9: Concentration profile for different values of N for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $Pr = 0.71$, and $Sc = 0.1$.

transfer decreases for both $\theta_r > 0$ and $\theta_r < 0$. From Figure 11, it is realized that as Le increases, the mass transfer increases for both $\theta_r > 0$ and $\theta_r < 0$.

The effect of Prandtl number Pr on velocity, temperature, and concentration is shown in Figures 12, 13, and 14, respectively, for $N = 1$, $Sc = 0.1$, $Du = 0.03$, $Sr = 2$, $Le = 0.1$, and $\theta_r = 5$. From Figures 12 and 13, it is evident that as the Prandtl number increases, the velocity and temperature increase. Figure 14 shows that as the prandtl number increases, the concentrations decrease.

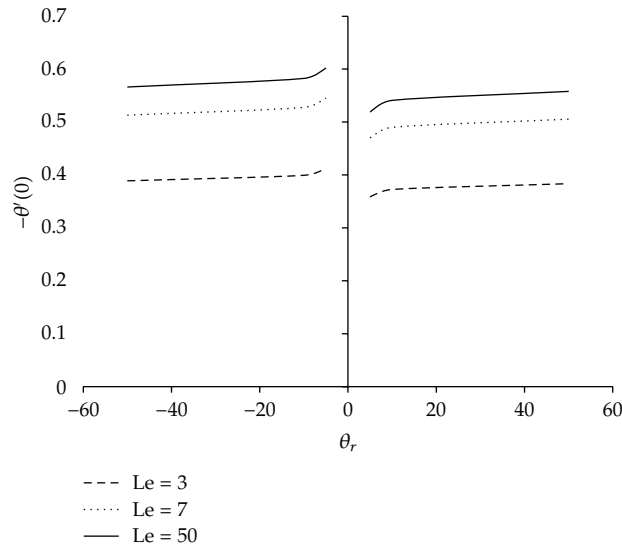


Figure 10: Effect of Lewis number Le on the rate of heat transfer for different values of θ_r for $Du = 0.03$, $Sr = 2$, $N = 1$, $Pr = 0.71$, and $Sc = 0.1$.

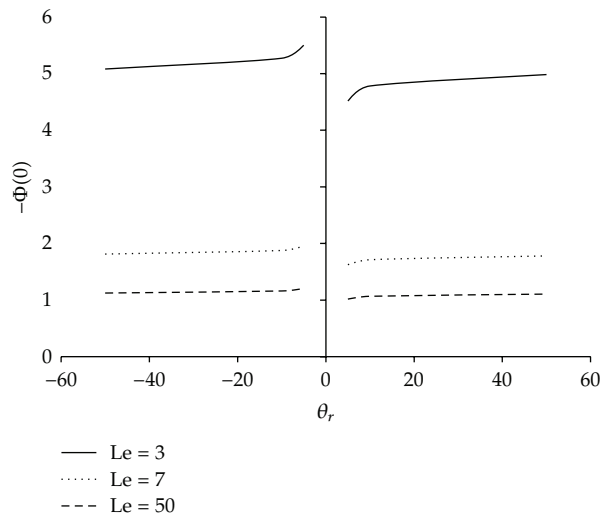


Figure 11: Effect of Lewis number Le on the rate of mass transfer for different values of θ_r for $Du = 0.03$, $Sr = 2$, $N = 1$, $Pr = 0.71$, and $Sc = 0.1$.

The parameters of engineering interests for the present problem are the local Nusselt number Nu_x and Sherwood number Sh_x , which are given by

$$\begin{aligned} \frac{Nu_x}{(Ra_x)^{1/2}} &= -\theta'(0) , \\ \frac{Sh_x}{(Ra_x)^{1/2}} &= -\phi'(0) . \end{aligned} \tag{4.1}$$

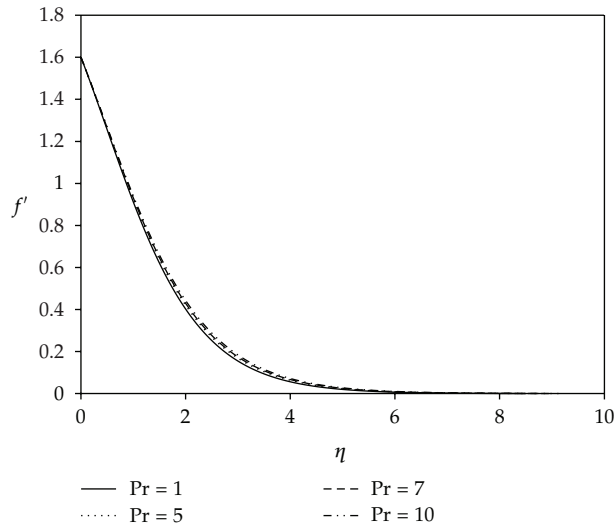


Figure 12: Velocity profile for different values of Pr for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $N = 1$, and $Sc = 0.1$.

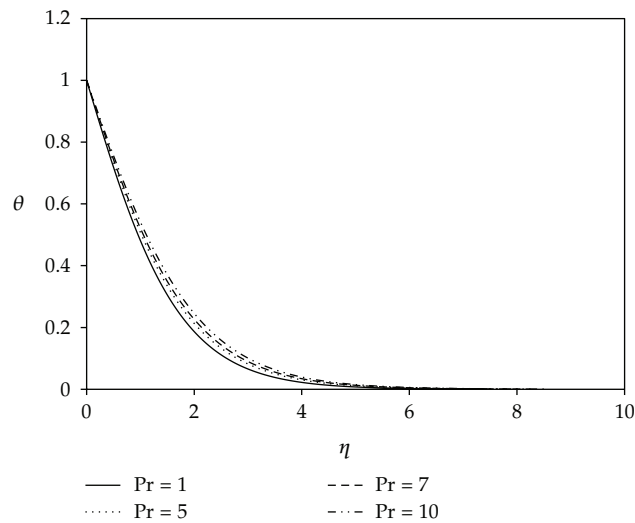


Figure 13: Temperature profile for different values of Pr for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $N = 1$, and $Sc = 0.1$.

The values of Nusselt number and Sherwood number for different values of variable viscosity θ_r and the buoyancy ratio N are presented in Table 1 for $Le = 0.1$, $Sc = 0.1$, $Du = 0.03$, $Sr = 2$, and $Pr = .71$. It is evident that as $\theta_r \rightarrow 0$ for $\theta_r > 0$, the Nusselt number decreases and the Sherwood number increases. It is also realized that as $\theta_r \rightarrow 0$ for $\theta_r < 0$, the Nusselt number increases and the Sherwood number decreases for other parameters fixed.

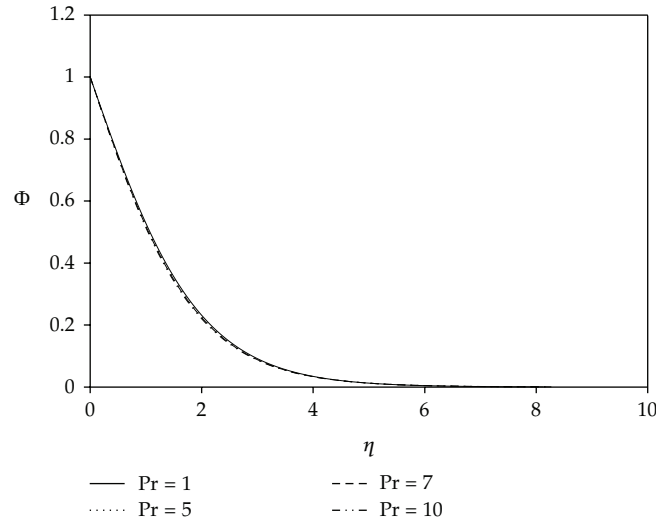


Figure 14: Concentration profile for different values of Pr for $Du = 0.03$, $Sr = 2$, $\theta_r = 5$, $Le = 0.1$, $N = 1$, and $Sc = 0.1$.

Table 1: Numerical values of Nusselt and Sherwood numbers for various values of N and θ_r for $Le = 0.1$, $Du = 0.03$, $Sr = 2$, $N = 1$, and $Sc = 0.1$.

θ_r	Nusselt number			Sherwood number		
	N					
	1	2	5	1	2	5
5	-0.6589	-0.8335	-1.2140	-0.0571	-0.0841	-0.1363
10	-0.6848	-0.8658	-1.2605	-0.0556	-0.0825	-0.1343
50	-0.7047	-0.8907	-1.2965	-0.0544	-0.0812	-0.1326
-5	-0.7568	-0.9558	-1.3903	-0.0514	-0.0779	-0.1283
-10	-0.7336	-0.9268	-1.3480	-0.0528	-0.0794	-0.1303
-50	-0.7145	-0.9029	-1.3140	-0.0539	-0.0806	-0.1318

5. Conclusion

The Dufour and Soret effect on free convective heat and mass transfer flow past a semi-infinite vertical plate under the influence of variable viscosity has been studied. Using usual similarity transformations, the governing equations have been transformed into nonlinear ordinary differential equations. The similarity solutions are obtained numerically by applying Runge-Kutta-Gill method along with shooting technique. The effects of the variable viscosity parameter θ_r , the Lewis number Le , the buoyancy ratio N , the Dufour number Du , the Soret number Sr , the prandtl number Pr , and the Schmidt number Sc on the velocity, temperature, and concentration profiles are examined. From the present study, we see that the thermal and species concentration boundary layer thickness increases for gases and decreases for liquids.

Nomenclature

- c : Concentration at any point in the flow field
 c_p : Specific heat at constant pressure
 c_s : Concentration susceptibility
 c_w : Concentration at the wall
 c_∞ : Concentration at the free stream
 D_m : Mass diffusivity
 Du : Dufour number
 f : Dimensionless velocity function
 g : Acceleration due to gravity
 k : Permeability
 k_T : Thermal diffusion ratio
 Le : Lewis number [$Le = \alpha/D_m$]
 N : Buoyancy ratio [$N = \beta^*(c_w - c_\infty)/\beta(T_w - T_\infty)$]
 Nu_x : Nusselt number [$Nu_x = -x(\partial T/\partial y)_{y=0}/(T_w - T_\infty)$]
 p : Pressure
 Pr : Prandtl number
 Ra_x : Rayleigh number $Ra_x = [kg\beta\Delta Tx/\nu\alpha]$
 Sc : Schmidt number
 Sh_x : Sherwood number [$Sh_x = mx/D(c_w - c_\infty)$]
 Sr : Soret number
 T : Temperature of the fluid
 T_w : Temperature of the plate
 T_∞ : Temperature of the fluid far from the plate
 u, v : Velocity components in x and y direction
 x, y : Coordinate system.

Greek Letters

- α : Thermal diffusivity
 β : Coefficient of thermal expansion
 β^* : Concentration expansion coefficient
 γ : Constant defined in (2.7)
 η : Dimensionless similarity variable
 θ : Dimensionless temperature
 θ_r : $-1/\gamma(T_w - T_\infty)$
 μ : Viscosity [pas]
 ν : Kinematic viscosity
 ρ : Density
 Φ : Dimensionless concentration
 ψ : Dimensionless stream function.

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